

# Agenda



# Linde's Hydrogen Portfolio

Linde's Hydrogen Fueling Technologies

**Deep Dive: Technical Optimisation** 

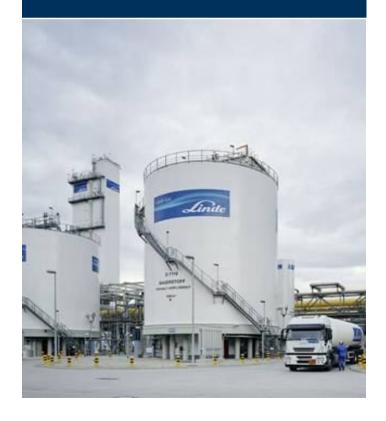
**Infrastructure Outlook** 

# The Linde Group: based on two pillars with extensive synergies



# The Linde Group

# Linde Gas



# Linde Engineering



# Our competence on hydrogen



# Linde covers the entire hydrogen value chain

# **Production** Conventional (e.g., SMR) Green (e.g., BTH)







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# Linde's advanced hydrogen fuelling technologies: Ionic compressor & cryo pump







### The Ionic Compressor

- High throughput of 33,6 kg/h at 900 bar<sup>1</sup>
- Energy consumption reduced by 25%<sup>2</sup>
- Very small number of moving parts (liquid piston)
- Reduced wear and long service life
- Fulfils industry standard SAE J 2601

# The Cryo Pump

- Very high throughput of up to 120 kg/h at 900 bar
- Energy consumption reduced by 70%<sup>2</sup>
- Small thermal management system
- High reliability, little maintenance effort and low costs
- Fulfils industry standard SAE J 2601

<sup>&</sup>lt;sup>1</sup> For one compressor. Modular setup allows for higher throughputs.

<sup>&</sup>lt;sup>2</sup> In comparison to a conventional piston compressor

# Reference projects prove technological maturity



### Linde reference projects



### **Key facts**

- More than 70 hydrogen stations equipped in 15 countries
- More than 350,000 successful fuellings
- Leading supplier of hydrogen fuelling technologies

### **Key Learnings**

- Technological maturity reached
- High level of standardisation reached
  - Standardised fuelling protocol SAE -J2601
  - Standardised H2 quality
- Comparable fuelling experience
  - 3 min / fuelling
  - Touch & feel like conventional stations
  - Integration into existing infrastructure

# Market Requirements on Hydrogen Fueling Infrastructure as a Series Product

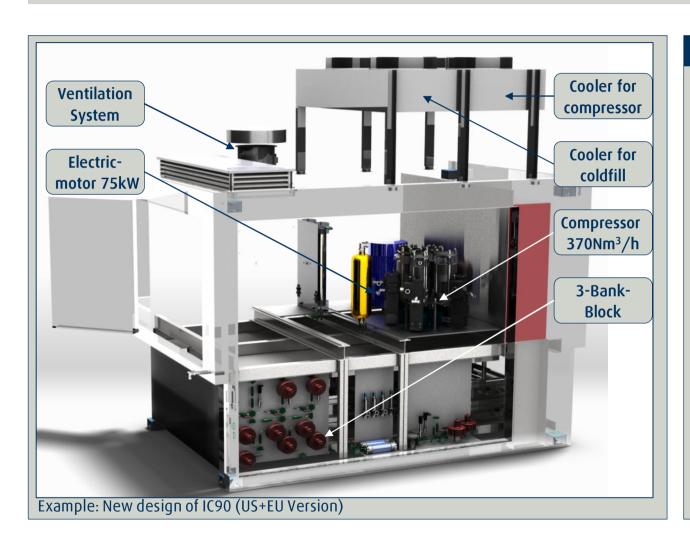


Market Requirement	Linde Technology
Small Footprint	<ul><li>System integration</li></ul>
Energy Efficiency	■ Efficient compression technologies and effective thermal management
Reliability	<ul><li>Use of durable components</li></ul>
Service & Maintenance	<ul> <li>Standardised service &amp; maintenance concepts including spare part management and technician service</li> </ul>
Low Capex/Opex	<ul> <li>Standardised and modular systems</li> </ul>
Steady further Development	■ Further technical optimisation

# IC90 for serial production

"IC90"



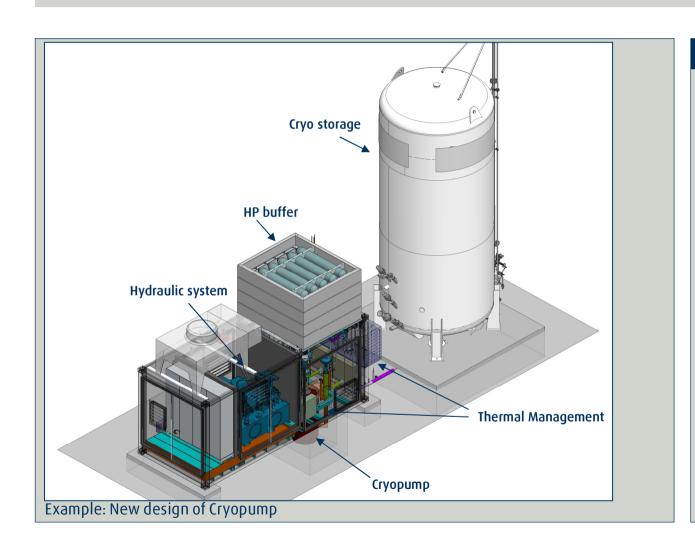


### Layout & performance

- Ionic compressor for H2
- Small footprint: 2,7m x 4,3m
- 5-stage compression
- Max. delivery rate: 370Nm3/h = 33,6kg/h
- Min. input: 5bara
- Max. output: 1.000bar
- Noise emission: <75dB(A)</p>
- Supply: gaseous or liquid
- Option for capacity upgrade(33,6kg/h = 67,2kg/h)
- Same container for US and EU model

# Standardized HFS Layout Cryopump





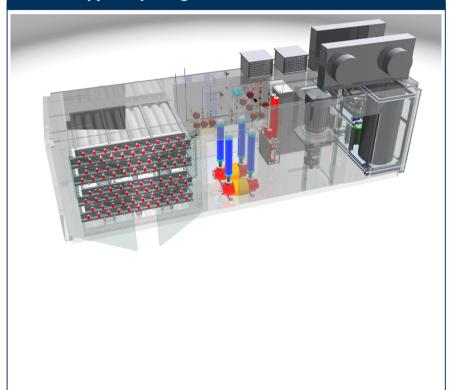
### **Facts**

- Cryopump for H2
- Small footprint: 20 ft' container
- 1-stage pressurization
- Max. delivery rate: 120kg/h
- Min. input: 2 bara
- Max. output: 900bar
- Noise emission: <74 dB(A)</p>
- Supply: liquid

# Development of HFS Size Ionic Compressor



# HFS, Type Hydrogear 2011: 30 ft Container

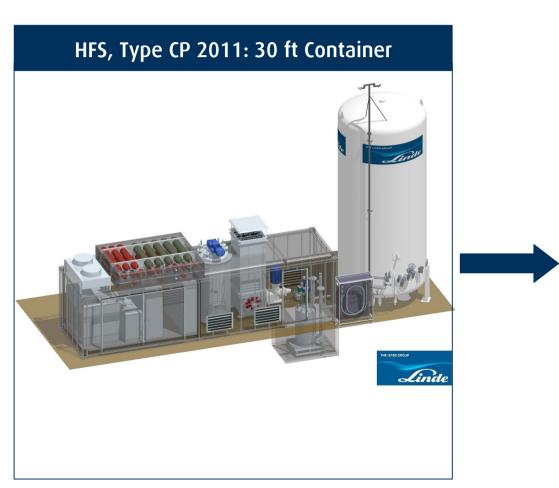


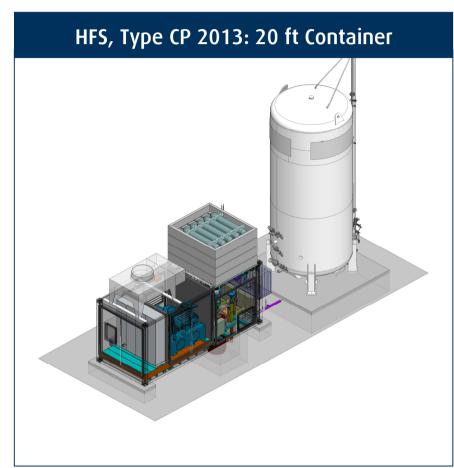
# HFS, Type IC90 2013: 14 ft Container



# Development of HFS Size Cryopump







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# Technical Optimisation Example: Optimisation of Cryopump Technology



### **Project Example:**

- Project "Further Development of the Cryopump Technology" since 04/2012
- Funding support of overall project by National Innovation Programme Hydrogen and Fuel Cell Technology (NIP)
- Linde AG Gases Division Hydrogen Solutions
- Ongoing PhD-Thesis on numerical simulation at Institute of Plant and Process Technology - Technische Universität München

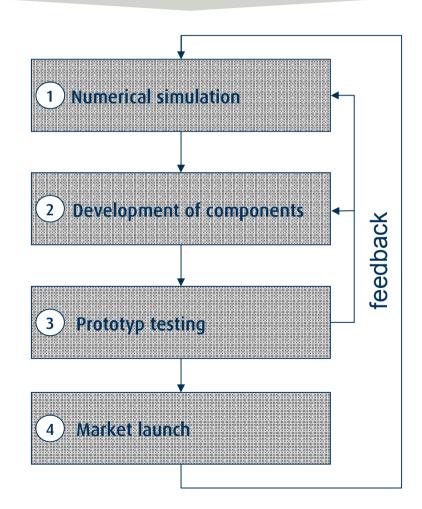
Gefördert durch:



Koordiniert durch:



### **Technical Optimisation Cycle**



# Numerical Simulation What is good for?



Result	Description
Knowledge	<ul> <li>Understanding of thermodynamical conditions</li> </ul>
Prediction	■ Prediction of system behaviour
Evaluation	■ Test and evaluation of new system designs
Optimisation	<ul><li>Optimise existing systems</li></ul>

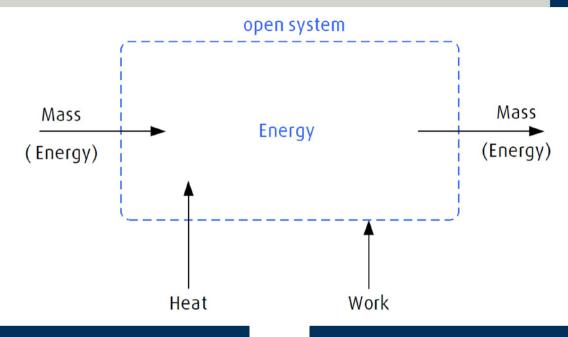
# Numerical Simulation Methodical Approach [1]



# Simulation target Prediction of thermal behaviour of the hydrogen fueling station Applicable model theory e. g. physical laws, equations of state Setup of mathematical equations Implementation in Matlab/Simulink-Software Check model validity Use of model for simulation target

# Mathematical Model Balance equations [1]



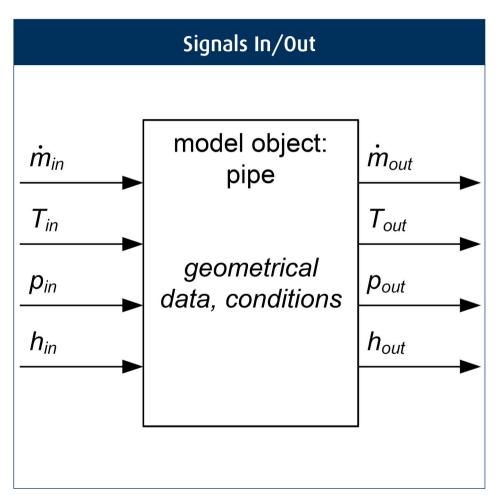


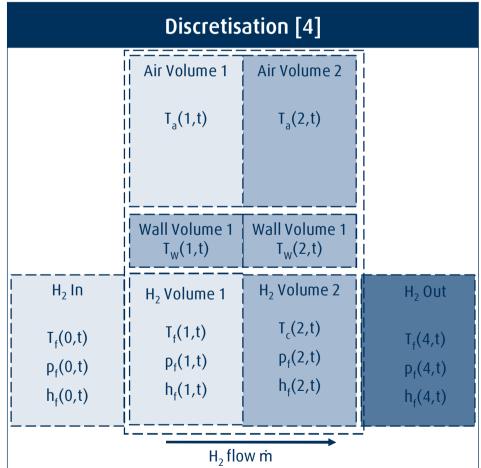
# Material Balance

# **Energy Balance**

# Mathematical Model Example: Pipe

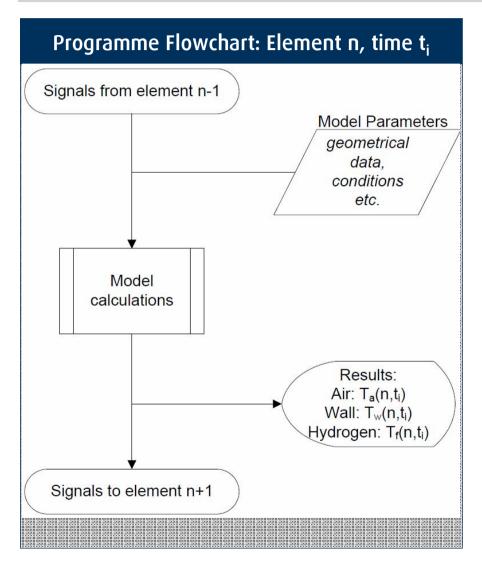


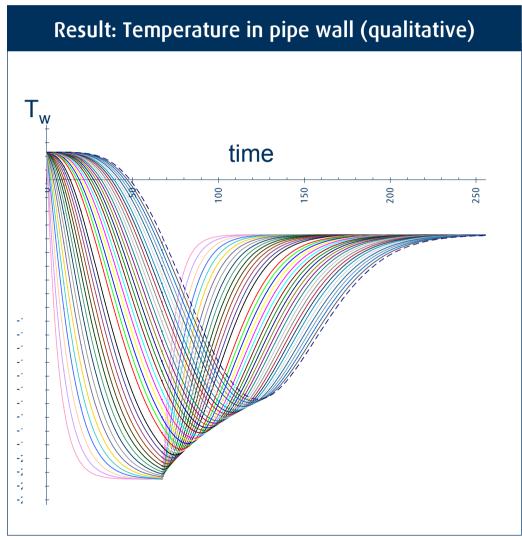




# Mathematical Model Example: Pipe







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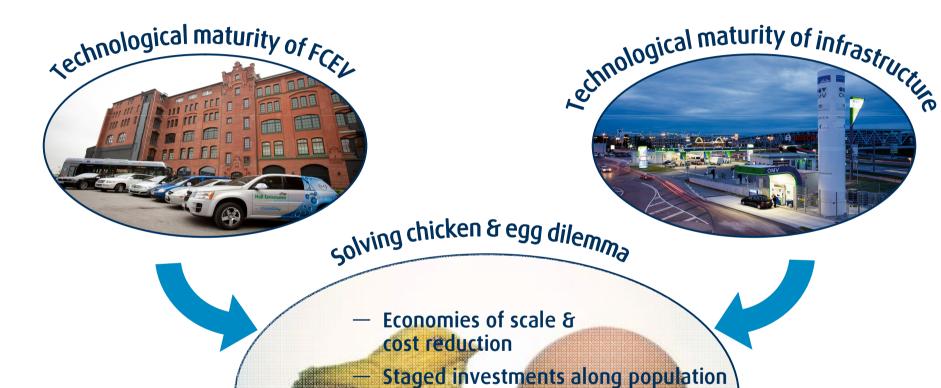
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# What is needed for a broad commercialization of hydrogen as fuel?





centres

Long-term partnerships

customer acceptance

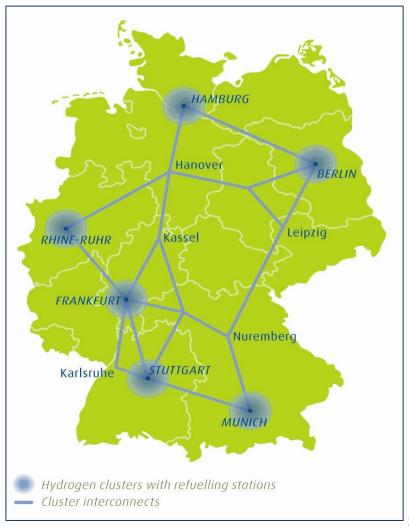
# Staged investments along population centres Linde & Daimler invest in 20 additional fuelling stations



### **Key facts**

- Initiative by Daimler and Linde
- Bridge the gap between demonstration
   (CEP) and commercialization (H2 Mobility)
- 10 + 10 additional public hydrogen stations in Germany
- Build-up from 2013 onwards
- Strengthen existing cluster and establish links
- Will allow to drive through Germany with hydrogen cars

### **Distribution of stations (preliminary)**



# Long-term partnerships **EU Study and H2 Mobility Initiative**



**EU hydrogen FCEV Coalition** 

H<sub>2</sub>-Mobility in Germany

**Investment and Business** Building

Goal

Fact-based evaluation of the potential of FCEV until 2050

**Integrated perspective** across hydrogen value chain

Business plan for roll-out of H2 infrastructure in Germany

Definition of technological standards

**Establishment** of "future consortium"

**Implementation** of comprehensive business case (incl. e.g., funding)

**Status** 

Finalized



Finalized-



















**Ongoing** 

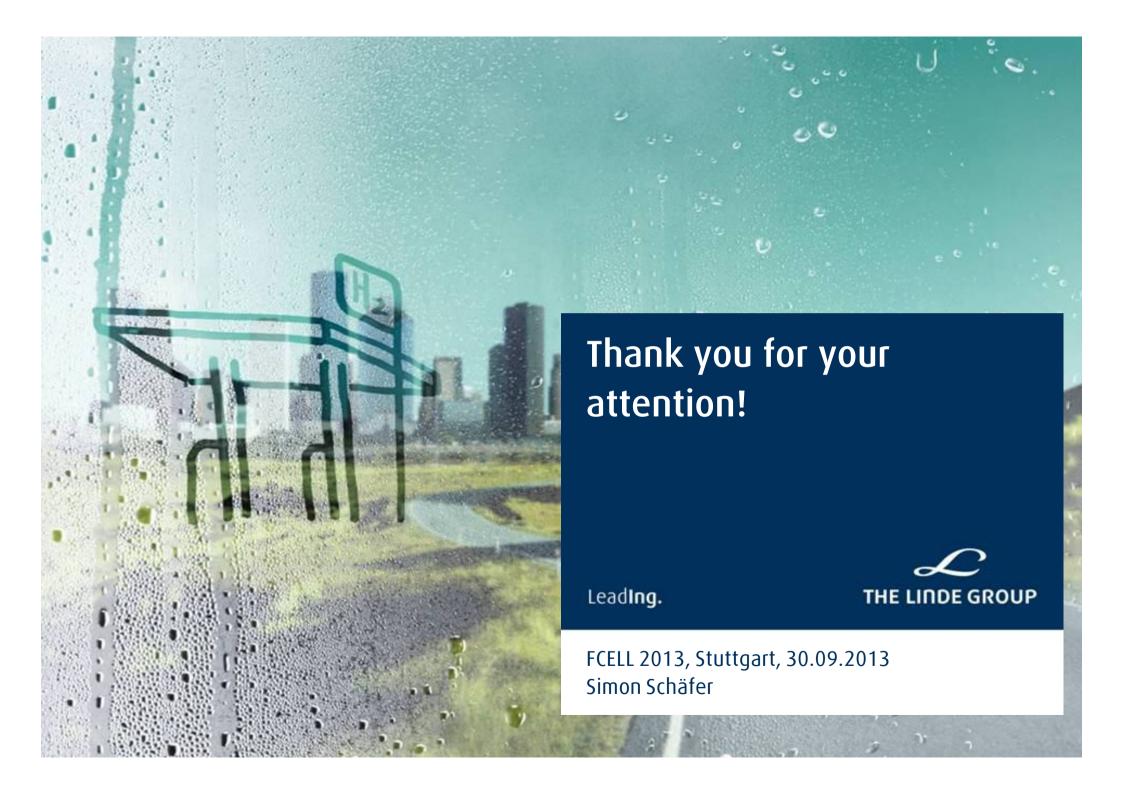


AIR LIQUIDE











1	Jürgen Gmehling: Chemical thermodynamics for process simulation. VCH,	
	Weinheim and and New York and and Basel and and Cambridge, 2006.	
2	Robert C. Reid, J. M. Prausnitz und Bruce E. Poling: <i>The properties of</i>	
	gases and liquids. McGraw-Hill, New York, 4 Auflage, 1987.	
3	J. W. Leachman, R. T. Jacobsen, S. G. Penoncello und E. W. Lemmon:	
	Fundamental Equations of State for Parahydrogen, Normal Hydrogen, and	
	Orthohydrogen. Journal of Physical and Chemical Reference Data, 38(3):721, 2009.	
4	David P. Hawn: Development of a a Dynamic Model of Counterflow Compact Heat Exchanger for Simulation of the	
	GT-MHR Recuperatur using Matlab and Simulink, Master Thesis , Ohio State University, 2009.	

# Backup



# **Mathematical Model** Equation of state (EOS)



**Equation of state** 

Formula

Adequacy

Ideal gas law

$$pv = RT$$

X

Peng-Robinson [2] 
$$p = \frac{RT}{v-b} - \frac{a\alpha}{v^2 - 2vb - b^2}$$

X

EOS by Leachman [3]

$$\phi(\tau, \delta) = \frac{f^{0}(T, \rho) + f^{r}(T, \rho)}{RT} = \phi^{0}(\tau, \delta) + \phi^{r}(\tau, \delta)$$

